Catalytic oxidation of propene over Pd catalysts supported on CeO₂, TiO₂, Al₂O₃ and M/Al₂O₃ oxides (M=Ce, Ti, Fe, Mn)

S. Gil ¹, L.F. Liotta*², G. Pantaleo², M. Ousmane³, L. Retailleau¹, A. Giroir-Fendler¹

*corresponding author: liotta@pa.ismn.cnr.it

Introduction

Propene is among the most investigated probe molecules in the field of VOC catalytic oxidation, because of its high photochemical ozone creativity potential (POCP) [1]. Supported noble metals (Pt, Pd, Au) show high activity for VOC oxidation, although their use is limited because of the high price and deactivation due to sintering of the active phase and poisoning effects [2]. It is well-known that the support nature plays an important role in improving the activity and durability of supported noble metals. For Pd supported catalysts the oxidation activity strongly depends on the acid-base properties of the support [3,4] as well as on the metal-support interaction [5]. In the present study, the catalytic oxidation of propene was investigated over Pd catalysts supported over CeO₂, TiO₂, Al₂O₃ and M/Al₂O₃ oxides (M=Ce, Ti, Fe, Mn). The propene oxidation activity of a conventional Pt/Al₂O₃, as reference, was also reported.

Materials and Methods

Commercial oxides, CeO₂ (Aldrich), TiO₂ (Eurotitania) and Al₂O₃ (Aldrich) were used as supports. Doped alumina oxides, M(5mol%)/Al₂O₃(95mol%), were prepared by wet impregnation with corresponding metal (Ce, Fe, Mn) nitrates or by grafting with Ti(iso-OC₃H₇)₄ in toluene solution and calcination at 500 °C for 3 h. Pd (0.8 wt%) and Pt (0.6 wt%) catalysts were prepared by impregnation method with Pd(NO₃)₂ and H₂PtCl₆ precursor, respectively. Then, the obtained powders were calcined at 400 °C for 4h. Characterizations by surface area measurements (BET method), X-ray diffraction (XRD), temperature programmed reduction/oxidation (TPR/TPO) and transmission electron microscopy (TEM) analyses were carried out. The activity tests were carried out in a tubular fixed-bed reactor under the reactive gas mixture containing 1000 ppm of C₃H₆ and 9% O₂ in He at GHSV of 35,000 h⁻¹.

Results and Discussion

In Fig. 1, TPR curves of selected catalysts, Pd/CeO_2 , Pd/TiO_2 and Pd/Al_2O_3 , are displayed. Peaks corresponding to different types of PdO species were observed at different temperatures depending on the support. Very small PdO particles were detected over TiO_2 . A second peak appearing at 8 °C, also observed for Pd/Al_2O_3 , was attributed to the reduction of bulky PdO particles [6]. For both catalysts, Pd/TiO_2 and Pd/Al_2O_3 , decomposition of β -hydride species takes place at 60 °C . Over CeO_2 , that is known to stabilize PdO, reduction occurred at higher temperature (25 °C). Moreover, a second peak, at 50 °C, ascribed to the reduction of ceria surface in contact with palladium was also observed.

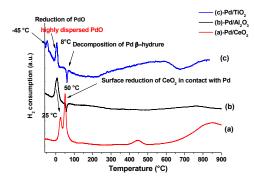


Fig. 1. TPR curves of Pd/CeO₂, Pd/Al₂O₃ and Pd/TiO₂ catalysts.

Above 300 °C CeO₂ and TiO₂ were reduced (surface reduction at around 400-500 °C, bulk reduction above 700 °C). In Fig. 2, the catalytic oxidation of C_3H_6 over Pd supported catalysts, in terms of reaction rate at 135 °C, is compared. The addition of Ce and Fe improved the catalytic activity of Pd supported catalysts, while no positive effect was played by 5% of Ti and Mn. Pd/CeO₂ was scarcely active as compared to Pd/TiO₂.

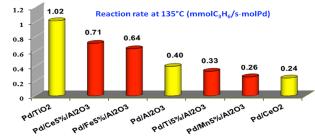


Fig. 2. Catalytic oxidation of C₃H₆ over Pd supported catalysts: reaction rate (mmol C₃H₆/s·mol Pd) calculated at 135 °C.

Significance: Pd/TiO_2 and $Pd/Ce5\%/Al_2O_3$ were the best performing catalysts. The lower activity of Pd/CeO_2 was likely due to the ceria effect which stabilizes PdO preferentially to the active site, metallic Pd.

References

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¹ Université de Lyon, Lyon, F-69003, France, Université Lyon 1, Villeurbanne, F-69622, CNRS, UMR 5256 IRCELYON, 2 avenue Albert Einstein, Villeurbanne, F-69622, France...

²Istituto per Lo Studio dei Materiali Nanostrutturati (ISMN)-CNR via Ugo La Malfa, 153, 90146 Palermo, Italy.

³ Rhodia China - E₂P₂L -UMI 3464, 3966 Jin Du Rd., (former 666 Shen Qiang Rd.,) Xin Zhuang Industrial Zone Shanghai 201108, China.