# Soot oxidation on Ag substituted LaMn<sub>0.9</sub>Co<sub>0.1</sub>O<sub>3.5</sub> perovskites

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## Introduction

Perovskites-type oxides, represented by the general formula  $ABO_3$  has been widely used in numerous applications due to their unique crystal structure, nonstoichiometric oxygen, acid-base property and redox properties. The number of potentially interesting perovskites in the oxidation reactions is very great, owing to the number of A and B cations that can enter into this structure. The partial substitution of the cation B by B' of similar oxidation state and ionic radius has been widely studied to improve perovskite stability or enhance its redox efficiency [1]. It is well known that the nature and the amount of the metal to be substituted in position A may also stabilize an unusual oxidation state of the cation in position B and/or produces oxygen vacancies .It is proposed to improve the activity or enhance the redox efficiency of  $LaMn_{0.90}Co_{0.1}O_3$  perovskite with low silver substitution substituting a trivalent cation, such as  $La^{3+}$  by a monovalent cation, such as  $Ag^+$  to be used calcined and reduced as catalysts on the catalytic combustion of soot.

#### Materials and Methods

The  $La_{1.x}Ag_xMn_{0.9}Co_{0.1}O_3$  ( $x_{Ag}$ = 0.0, 0.1, 0.2, 0.3) perovskites were prepared by the citrate method, calcined at 700 °C and characterized by nitrogen adsorption, XRD, SEM, TPR, O<sub>2</sub>-TPD and XPS. The catalytic activity of the calcined and reduced perovskites was studied using carbon black, CB, as a model of soot. The catalyst and carbon black mixture for the assessment of the catalytic activity was prepared mixing 4 mg of CB and 16 mg of catalyst in tight contact. The catalytic oxidation of soot was carried out in a thermogravimetric apparatus (Netzch 409 PC) with 7.5 mg of the mixture heated in 180 mL min<sup>-1</sup> flow of 12%O<sub>2</sub>/He at 10°C min<sup>-1</sup> up to 800°C.

#### Results and Discussion

The catalytic activity was estimated from the temperature corresponding to the maximum of DTG curve, Tm, shown in Table 1. Higher values for Tm mean lower catalytic activity. The Tm for the uncatalized CB combustion is  $650^{\circ}$ C, so all tested samples exhibit a significant catalytic activity; increasing with Ag content [2]. The BET specific areas do not show significant differences with Ag content, while a large decrease, ~ 40 to 50%, upon the reductive treatment almost independent of the Ag content can be detected, Table 1. The XRD patterns of the calcined perovskites reveal that the rhombohedral-hexagonal structure is obtained for the LaMn<sub>0.9</sub>Co<sub>0.1</sub>O<sub>3</sub> and low Ag substituted ( $x_{Ag}$ = 0.1 and 0.2) samples, however a certain drop of crystallinity is observed for  $x_{Ag}$ =0.3. After the reductive treatment, the silver-substituted perovskites show three diffraction lines of increasing intensity upon Ag substitution at 20 values of 37.96°, 44.14° and 64.30°. The close proximity of the strongest diffraction lines of Ag° (JCPDS 04-0783) and Ag<sub>2</sub>O (JCPDS 12-793) made very difficult. if not

impossible, to unequivocally identify the oxidation state of the bulk silver. The  $Ag_2O$  mean crystal size evaluated by using the Debye Scherrer equation at  $2\theta$ =37.96° is shown in Table 1. The TPR profiles indicates a first reduction ascribed to the reduction of the network with the formation of oxygen-deficient perovskite and a shoulder corresponding to the reduction of segregated  $Mn^{4+}$  oxide. A second reduction stage, starting at 650°C, corresponds to the formation of  $Co^0$  and MnO phases and the consequently destruction of the perovskite structure. The peak's shift towards lower temperatures indicates a growth in crystal size.

Table 1 Surface area, crystal size and temperature at the maximum rate combustion, Tm, for La<sub>1-x</sub>Ag<sub>0x</sub>Mn<sub>0.9</sub>Co<sub>0.1</sub>O<sub>3</sub> perovskites.

|  | $S_{BET,} m^2 g^{-1}$ |         | $d_{hkl}$ $Ag_2O$ , $nm$ |         | T <sub>m</sub> , °C |         |
|--|-----------------------|---------|--------------------------|---------|---------------------|---------|
|  | calcined              | reduced | calcined                 | reduced | calcined            | reduced |
| $LaMn_{0.9}Co_{0.1}O_3$                    | 29                    | 15      | 0.0                      | 0.0     | 458                 | 459     |
| $La_{0.9}Ag_{0.1}Mn_{0.9}Co_{0.1}O_{3} \\$ | 27                    | 17      | 26                       | 43      | 430                 | 459     |
| $La_{0.8}Ag_{0.2}Mn_{0.9}Co_{0.1}O_{3} \\$ | 30                    | 16      | 29                       | 42      | 394                 | 422     |
| $La_{0.7}Ag_{0.3}Mn_{0.9}Co_{0.1}O_{3} \\$ | 30                    | 18      | 29                       | 45      | 371                 | 419     |

Three different surface oxygen species were detected by XPS for the Ag-substituted perovskites: (i), surface lattice oxygen species ( $O_{latt}^2$ ) at 529.8 eV; (ii), weakly adsorbed oxygen species ( $O_{ads}$ ) such as hydroxyl and/or carbonate groups at 531.0–531.4 eV; and (iii), loosely adsorbed superperoxide species ( $O_{2ads}$ ) species at 532.4–532.6 eV . The appearance of  $O_2$  super oxides pecies at binding energies higher than 532 eV, is a consequence of the lower oxidation state of the  $Ag^+$  inserted into the network

## Significance

The high increase in the catalytic activity at higher Ag substitution suggest that the activity of these materials for soot combustion is improved by two factors: i) the increasing of surface oxygen species content, closely related to higher material capacity for oxygen transfer from catalyst to carbonaceous surface and ii) the formation of  $Ag_2O$  crystals for the higher-Agcontent perovskites. The high thermal resistance of the perovskite-type structure upon a reductive process decreases the catalytic activity for soot combustion due to both a sintering  $Ag_2O$  process and a decrease in the surface area entailing a decrease of the oxygen exchange and the number of contact points between catalyst and soot.

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### References

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